Crushing
Optimizing the Process

QUARRY ACADEMY

Improving Processes. Instilling Expertise.
Optimizing the Process

• Methods to combine and simulate technical and economic performance
• Optimum crushing plant performance is difficult to achieve due to the process characteristics. Different compared to all other industrial processes.
• Optimizing method for best performance
• Partly implemented in PlantDesigner 10
Crushing Plant Optimization

- Point of interest
  - Crushing stage
  - Crushing plant
  - Quarry Process

- Today:
  - Optimize the feed
  - Optimize the process
Optimization of a Final Crushing Stage

- Who is control of your process performance?
- What tools have been provided to make the production efficient?

- Maximize crusher yield
  - Production of valuable products
  - Efficient production of current product demands

- *Crusher Performance Map* will help guide the crusher operator
Optimization of a Final Crushing Stage

- This method applies to other crushers where a control variable is available.
- The crushers are the last size reduction stage in the value chain.
- Over crushing is common.
- The connection between crusher setting and yield is often unknown.
- The rock cannot be repaired.
- We need to control the crusher carefully.
Optimization of one parameter (CSS) can be done by sampling and analysis.

The invested time and lost production will quickly be repaid by increased productivity.

Combine product yield and economic aspects.

This can be done by taking samples and making the analysis in MS Excel.
Optimization of a Final Crushing Stage

- Material from crusher is sampled
- Measure the capacity at each crusher settings. CSS will effect the final product capacity, especially in a closed circuit.
- Production of 4 valuable products
  - 0.08-0.16” (2-4 mm)
  - 0.16-0.32” (4-8 mm)
  - 0.32-0.64” (8-16 mm)
  - 0.64-0.87” (16-22 mm)
- By-product with no value
  - 0-0.08” (0-2 mm)
Optimization of a Final Crushing Stage

- Run the crusher at different settings
- Take at least one sample at each setting. (Multiple samples are often useful)

- Special Attention to Safety when taking samples!!
- Position of point were samples are taking.
- Ensure that the conveyor will not start by accident.
Optimization of a Final Crushing Stage

- Particle Size Distribution Plots
- If taking single samples on each CSS the risk of getting inconsistent results might make the graph look strange.

- Impossible to determine optimum setting by only using particle size distribution graphs.
Optimization of a Final Crushing Stage

- If taking single samples on each CSS the risk of getting inconsistent results might make the graph look strange.
- Impossible to determine optimum setting by only using particle size distribution graphs.
• Combine the particle size distribution and capacity.
• Percentage of final product times the capacity gives the production capacity of each product.

• Example 0.08”-0.16” mm at CSS 0.79”:
  – Percentage of crusher production
  – 20% - 11% = 9%
  – Crusher capacity
  – 193 tph

  – Total Production:
  – 193 tph x 9% = 17 tph
Optimization of a Final Crushing Stage

- Entering all the values into MS Excel makes this easy to get production capacities.
- Still difficult to determine the optimal setting.

![Crusher Production Chart]

- CSS ['

Crusher Production

Production Capacity [tph]

CSS ['']

0-0.08
0.08-0.16
0.16-0.32
0.32-0.64
0.64-0.87
Optimization of a Final Crushing Stage

- Use the price* per ton for all products:
  - 0-0.08”: $0 (by-product)
  - 0.08-0.16”: $12.30
  - 0.16-0.32”: $13.85
  - 0.32-0.64”: $16.90
  - 0.64-0.87”: $10.80

- Make an income graph by combining prices with capacity

*All prices are estimates based on publicly available data
**Optimization of a Final Crushing Stage**

- **What difference does it make?**
  - Running the crusher 0.08” off:
    - Decrease the profit by 58.5 $/h
    - Running the crusher at 1600 hours per year:
      \[ 58.5 \times 1600 = 93600 \]

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**Crusher Yield**

- **Optimization:**
  - The effort put in to optimization will repay itself quickly
Crusher Performance Map

• The general idea:
  – Select a crusher where you think optimization will be beneficial
  – Make a plan for what you would like to test
    • CSS, Speed, Curtain Position…
  – Run a sampling campaign
    • Particle size distribution, shape, capacity
  – Do the analysis
    • Convert test results into values of performance
  – Find the sweet spot
Crusher Performance Map

The Crusher Performance Map can assist your operator with maintaining efficient production.
MinBaS II
Optimized blasting

Field Study in Långåsen, Arlanda

• Aim: Evaluate the effect of using electronic blasting systems. Changes in particle size distribution and other benefits.
  • Full scale testing. Four blasts blasted during 2008
  • Based on the final report and my own observations
  • All data and costs shown are estimates based on publically available data
The Study

• Comparisons between the cost and earnings for different blasting strategies.
• Conclusions and recommendations
The Quarry
Långåsen, Arlanda

- Operated by NCC Roads
- Capacity 300-400 tph
- Aggregates and Asphalt Production
- Contractor for transportation of blasted material to primary crusher
- Contractor owns and operates the C&S plant
# Blasted Material Test plan

<table>
<thead>
<tr>
<th>Blast</th>
<th>Type</th>
<th>Explosive Use</th>
<th>Charge Density 1</th>
<th>Charge Density 2</th>
</tr>
</thead>
<tbody>
<tr>
<td>Blast 1</td>
<td>None Electric</td>
<td>None Electric</td>
<td>1.35 lb/yd³</td>
<td>1.85 lb/yd³</td>
</tr>
<tr>
<td>Blast 2</td>
<td>None Electric</td>
<td>None Electric</td>
<td>1.85 lb/yd³</td>
<td>1.35 lb/yd³</td>
</tr>
<tr>
<td>Blast 3</td>
<td>Electronic Blasting System</td>
<td></td>
<td>1.35 lb/yd³ 10 ms between holes</td>
<td></td>
</tr>
<tr>
<td>Blast 4</td>
<td>Electronic Blasting System</td>
<td></td>
<td>1.35 lb/yd³ 5 ms between holes</td>
<td></td>
</tr>
</tbody>
</table>
Blasting result

Measuring the Particle Size Distribution

Andel passerar, %

- Nonel, q = 0.72 kg/m³
- Nonel, q = 0.99 kg/m³
- Nonel-kurv design
- EPD, q = 0.78 kg/m³
- EPD-kurva C3
# Blasting result
## Cost analysis

<table>
<thead>
<tr>
<th></th>
<th>Nonel norm. q [$/ton*]</th>
<th>Nonel high q [$/ton*]</th>
<th>EPD norm. q [$/ton*]</th>
</tr>
</thead>
<tbody>
<tr>
<td>Drilling and Blasting</td>
<td>0.90</td>
<td>1.23</td>
<td>0.97</td>
</tr>
<tr>
<td>Added cost for detonators</td>
<td>0.00</td>
<td>0.00</td>
<td>0.30</td>
</tr>
<tr>
<td>Bolder Management</td>
<td>0.30</td>
<td>0.15</td>
<td>0.22</td>
</tr>
<tr>
<td><strong>Sum</strong></td>
<td><strong>1.20</strong></td>
<td><strong>1.38</strong></td>
<td><strong>1.49</strong></td>
</tr>
</tbody>
</table>

*Estimates based on publicly available data*
Loading and Hauling Conditions and Measurements

- **Loading and Hauling to primary crusher**
  - Wheel loader carries the material from the muck pile to the crusher

- **Conducted studies**
  - Measurement of wheel loaded loading times
  - Measurement of loaded material [tph]
  - Manual timing during several days
## Loading and Hauling

### Cost analysis

<table>
<thead>
<tr>
<th></th>
<th>Nonel norm. q</th>
<th>Nonel high q</th>
<th>EPD norm. q</th>
</tr>
</thead>
<tbody>
<tr>
<td>Contractor [$/h*]</td>
<td>448</td>
<td>448</td>
<td>448</td>
</tr>
<tr>
<td>Loading Capacity [tph]</td>
<td>298</td>
<td>316</td>
<td>313</td>
</tr>
<tr>
<td>Cost [$/ton]</td>
<td>1.50</td>
<td>1.42</td>
<td>1.43</td>
</tr>
<tr>
<td>Sum incl Drilling and Blasting [$/ton]</td>
<td>1.20+1.50=2.70=</td>
<td>1.38+1.42=2.80=</td>
<td>1.49+1.43=2.92=</td>
</tr>
</tbody>
</table>

*Estimates based on publicly available data
Crushing and Screening Plant Setup and Conditions for the Study

0-3.5” (0-90 mm) +3.5” (+90 mm)
Crushing and Screening
Performed Measurements

Power Draw [kwh]

Capacity [tph]

0-3.5"
+3.5"
## Crushing and Screening Cost analysis

<table>
<thead>
<tr>
<th></th>
<th>Nonel norm. q</th>
<th>Nonel high q</th>
<th>EPD norm. q</th>
</tr>
</thead>
<tbody>
<tr>
<td><strong>Power Draw (kWh/ton)</strong></td>
<td>0.3</td>
<td>0.25</td>
<td>0.35</td>
</tr>
<tr>
<td><strong>Energy Cost (0.30 $/kWh)</strong>*</td>
<td>0.09</td>
<td>0.07</td>
<td>0.10</td>
</tr>
<tr>
<td><strong>Fixed Cost [$/h]</strong></td>
<td>746</td>
<td>746</td>
<td>746</td>
</tr>
<tr>
<td></td>
<td>2.41</td>
<td>2.29</td>
<td>2.28</td>
</tr>
<tr>
<td><strong>Cost [$/ton]</strong></td>
<td>2.50</td>
<td>2.36</td>
<td>2.38</td>
</tr>
<tr>
<td><strong>Sum incl D&amp;B och L&amp;H [$/ton]</strong></td>
<td>1.20+1.50+2.50=</td>
<td>1.38+1.42+2.36=</td>
<td>1.49+1.43+2.38=</td>
</tr>
<tr>
<td></td>
<td>= 5.20</td>
<td>= 5.16</td>
<td>= 5.30</td>
</tr>
</tbody>
</table>

*Estimates based on publicly available data
# Production

## Total cost $/h

<table>
<thead>
<tr>
<th></th>
<th>Nonel norm. q</th>
<th>Nonel high q</th>
<th>EPD norm. q</th>
</tr>
</thead>
<tbody>
<tr>
<td>Production rate [tph]</td>
<td>298</td>
<td>316</td>
<td>313</td>
</tr>
<tr>
<td>Cost [$/h]</td>
<td>1600</td>
<td>1676</td>
<td>1723</td>
</tr>
</tbody>
</table>

Distribution between 0-3.5” and +3.5” is partly controlled by the blasting result.
### Procution Product Price

<table>
<thead>
<tr>
<th></th>
<th></th>
<th></th>
<th></th>
</tr>
</thead>
<tbody>
<tr>
<td>0-90</td>
<td>11.94</td>
<td>1 (Prim.)</td>
<td>11.94</td>
</tr>
<tr>
<td>0-4</td>
<td>19.25</td>
<td></td>
<td></td>
</tr>
<tr>
<td>4-8</td>
<td>20.75</td>
<td>3-4</td>
<td>21.19</td>
</tr>
<tr>
<td>8-11</td>
<td>23.73</td>
<td></td>
<td></td>
</tr>
<tr>
<td>11-16</td>
<td>22.53</td>
<td></td>
<td></td>
</tr>
<tr>
<td>16-32</td>
<td>20.15</td>
<td></td>
<td></td>
</tr>
</tbody>
</table>

*Estimates based on publicly available data*
# Production Revenue sek/h

<table>
<thead>
<tr>
<th></th>
<th>Nonel normalt q</th>
<th>Nonel high q</th>
<th>EPD normalt q</th>
</tr>
</thead>
<tbody>
<tr>
<td>Production [tph]</td>
<td>298</td>
<td>316</td>
<td>313</td>
</tr>
<tr>
<td>Production 0-3.5” [tph]</td>
<td>186</td>
<td>206</td>
<td>189</td>
</tr>
<tr>
<td>Price 0-3.5” $/ton*</td>
<td>11.94</td>
<td>11.94</td>
<td>11.94</td>
</tr>
<tr>
<td>Production +3.5” [tph]</td>
<td>112</td>
<td>110</td>
<td>124</td>
</tr>
<tr>
<td>Revenue $/h</td>
<td>4595</td>
<td>4791</td>
<td>4885</td>
</tr>
</tbody>
</table>

*Estimates based on publicly available data
Production Cost and Revenue*

<table>
<thead>
<tr>
<th></th>
<th>Nonel norm. q</th>
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<th>EPD norm. q</th>
</tr>
</thead>
<tbody>
<tr>
<td>Production rate [tph]</td>
<td>298</td>
<td>316</td>
<td>313</td>
</tr>
<tr>
<td>Cost [$/h]</td>
<td>1343</td>
<td>1412</td>
<td>1425</td>
</tr>
</tbody>
</table>

*Based on publicly available data

Minimizing cost does not necessarily profit

Distribution between 0-3.5” and +3.5” is partly controlled by the blasting result
Conclusions

• From the tested blasting alternative Electronic Blasting System is the most beneficial.

• Extensive investigations and analysis are necessary in order to determine the optimal solution. Many areas are affected by the blasting result.
  – Drilling and Blasting
  – Bolder Management
  – Loading and Hauling
  – Crushing and Screening

• Only studying the costs is not sufficient in order to optimize the process. Most expensive solution did also generate the most profit.
Conclusions – Guidance for previous processes

• Feed to the primary crusher matters more than just boulders.
• The effect of different feed gradations (blast results) are difficult to detect without measuring actively.
• Communicate effects upwards in the process.
What about Optimizing the Crushing and Screening Process?

• Optimizing a single crusher can be done manually as seen earlier

• Optimizing several crushers?
  – Combination of equipment setting
  – Production situation, what products are demanded and what are not?
Crushing plant optimization using TCO

Objective of project

• To optimize the crushing plant using computer optimization
• Use sampling to calibrate the computer model in order to increase model accuracy
• Optimize with the goal to maximize gross profit
Yield the most profitable production strategy and meet the market demand

Optimization cannot be done without including economics
Crushing plant optimization using TCO Calculation approach

- Included in cost the calculation
  - Raw material
  - Depreciation
  - Interest
  - Energy cost
  - Wear parts replacement
  - Service cost
  - By-product production
  - Personnel

- Income calculation
  - Sellable products
  - Product demand

- Other factors included that effects the gross profit
  - Availability
  - Utilization
Crushing plant optimization using TCO
Plant Challenges

What is the best trade-off between capacity and reduction?
Crushing plant optimization using TCO Test plant

In normal production following CSS are utilized:

Secondary crusher – CSS 44 mm 1.73”
Tertiary crusher – CSS 16 mm 0.63”
Quaternary crusher – CSS 13 mm 0.51”

Products:

- 0-2 mm
- 2-5 mm
- 5-8 mm
- 8-11 mm
- 11-16 mm
- 16-22 mm

0-0.9”
Crushing plant optimization using TCO

Test plan

Objectives for the first test session:

• Measure particle size distribution to calibrate the simulation model
• CSS at original settings
Crushing plant optimization using TCO Model Calibration
Crushing plant optimization using TCO
Running the TCO optimization module

The computer tool automatically finds the best solution using an optimization algorithm
The solution that yields the best profit:

• Secondary crusher – CSS 50 mm (44), 1.96” (1.73”)
• Tertiary crusher – CSS 20 mm (16) 0.78” (0.63”)
• Quaternary crusher – CSS 14 mm (13) 0.55” (0.51”)

[Diagram of a crushing plant]
Crushing plant optimization using TCO

Results

Result: +11 % in Calculated Gross Profit

- Increased Capacity
- Reduced fines ratio
- Increased total production

Calculated Gross Profit
Crushing plant optimization using TCO
How can it be done?
Crushing plant optimization using TCO

Conclusion

• Optimization must be a combination of technical and economic analysis
• Computer optimization can improve productivity
• Model calibration increases accuracy
• Minimizing cost does not necessarily maximize profit
• Combined performance of different machines should be considered. Solves the trade-off between capacity and reduction