



Hydraulic Evaluation of an Off-Shore Pumping Station

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PEMEX Exploracion y Produccion

Outline



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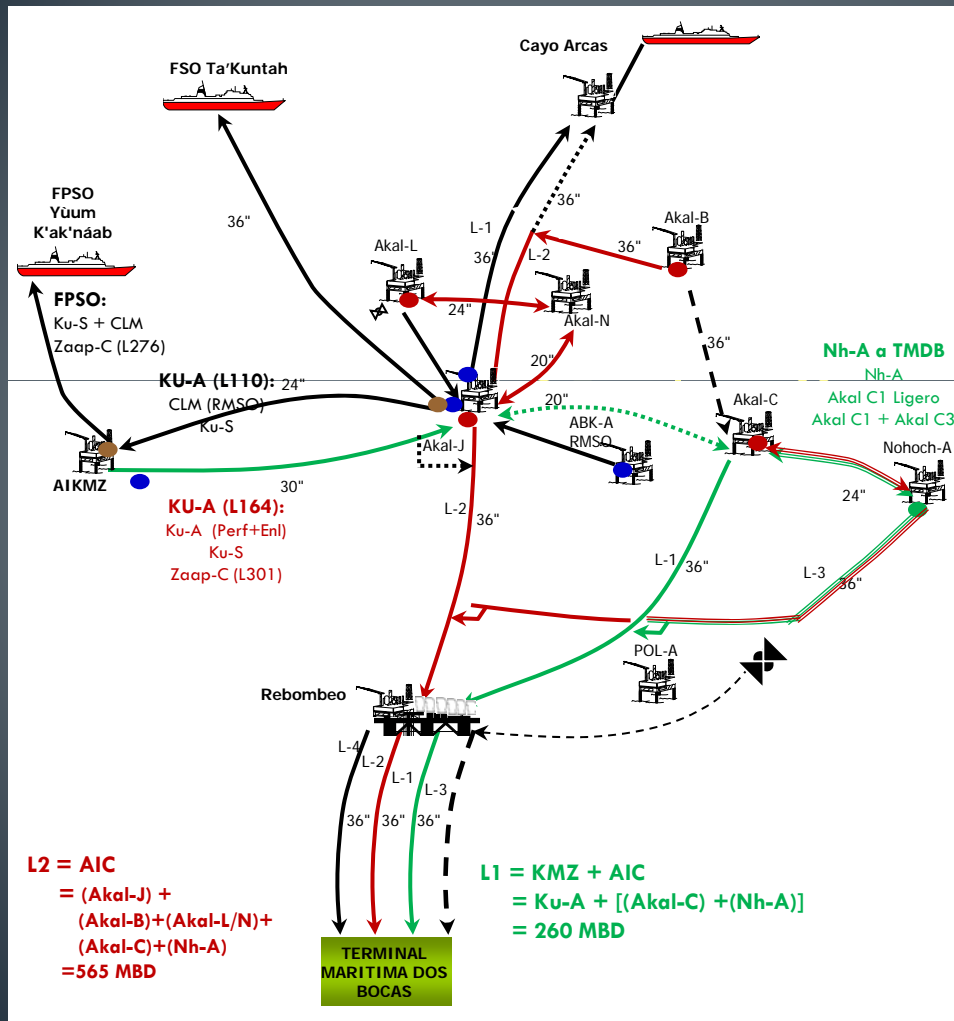
Background



- PEMEX Exploration and Production off-shore pumping system transports between 46%-52% of the national crude oil production.
- The current system operates with crude oils in the range of 19° API, expected new mixtures of approximately 16° API.
- Complex interconnected platform network where different crude oils are mixed and pumped into various pipelines.
- An upgrade of the facility and pumping equipment is required to handle new crude oil mixtures (16° API).



Introduction

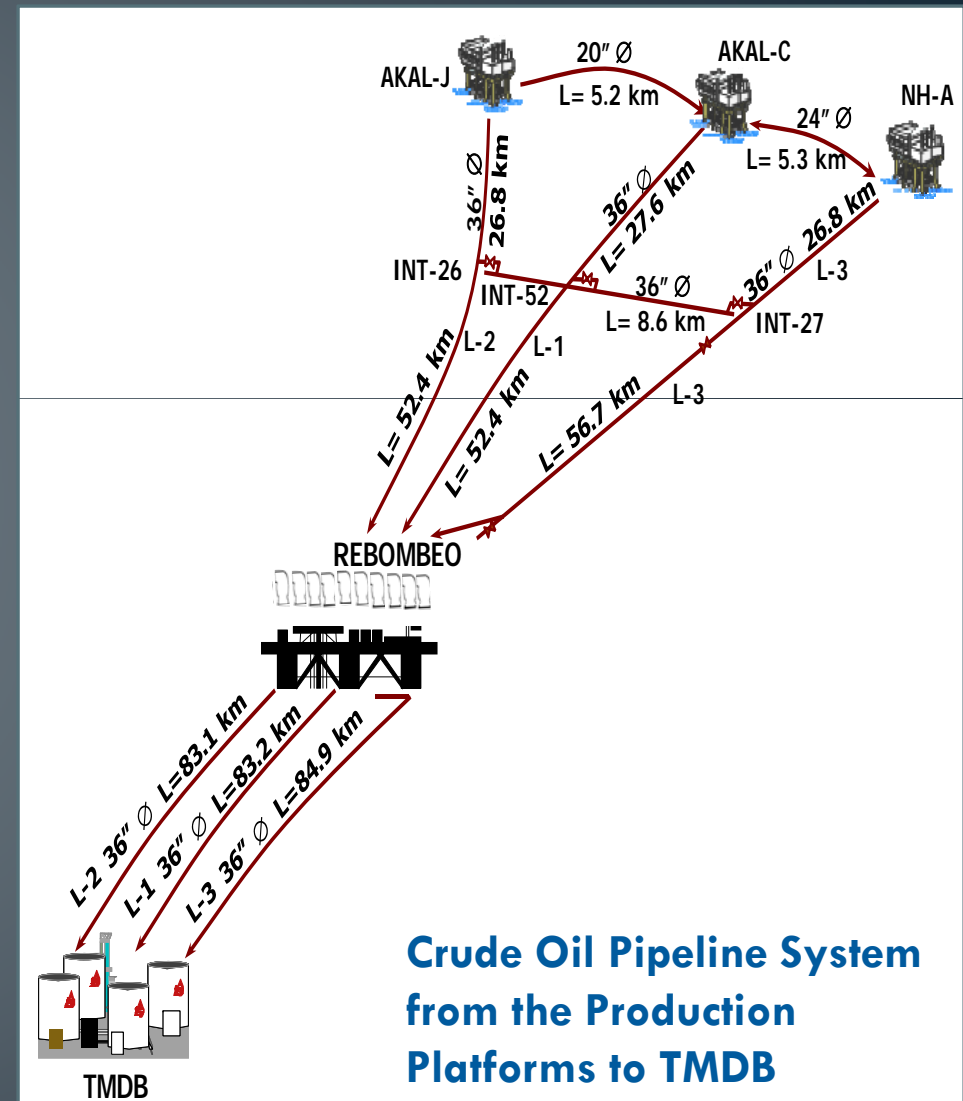


- Two 36-inch sub-sea pipelines travel 52 miles.
- The booster platform “Rebombeo” is located in the Gulf of Mexico approximately 25 miles off-shore. ➔
- Crude oil production from several platforms is collected and transported (19-21° API crude oil emulsions).
- Ten centrifugal pumps are installed in the booster platform.

Pipeline Model



- 1-D pipeline fluid model of the existing facility including L1, L2, and L3 lines.
- Field measurements of the pump performance curves.
- Various emulsion of water-in-oil up to 30% water-cut.
- Flow, pressure, and temperature field data was used to validate the hydraulic model within 1.12%.



Emulsions Viscosity Model



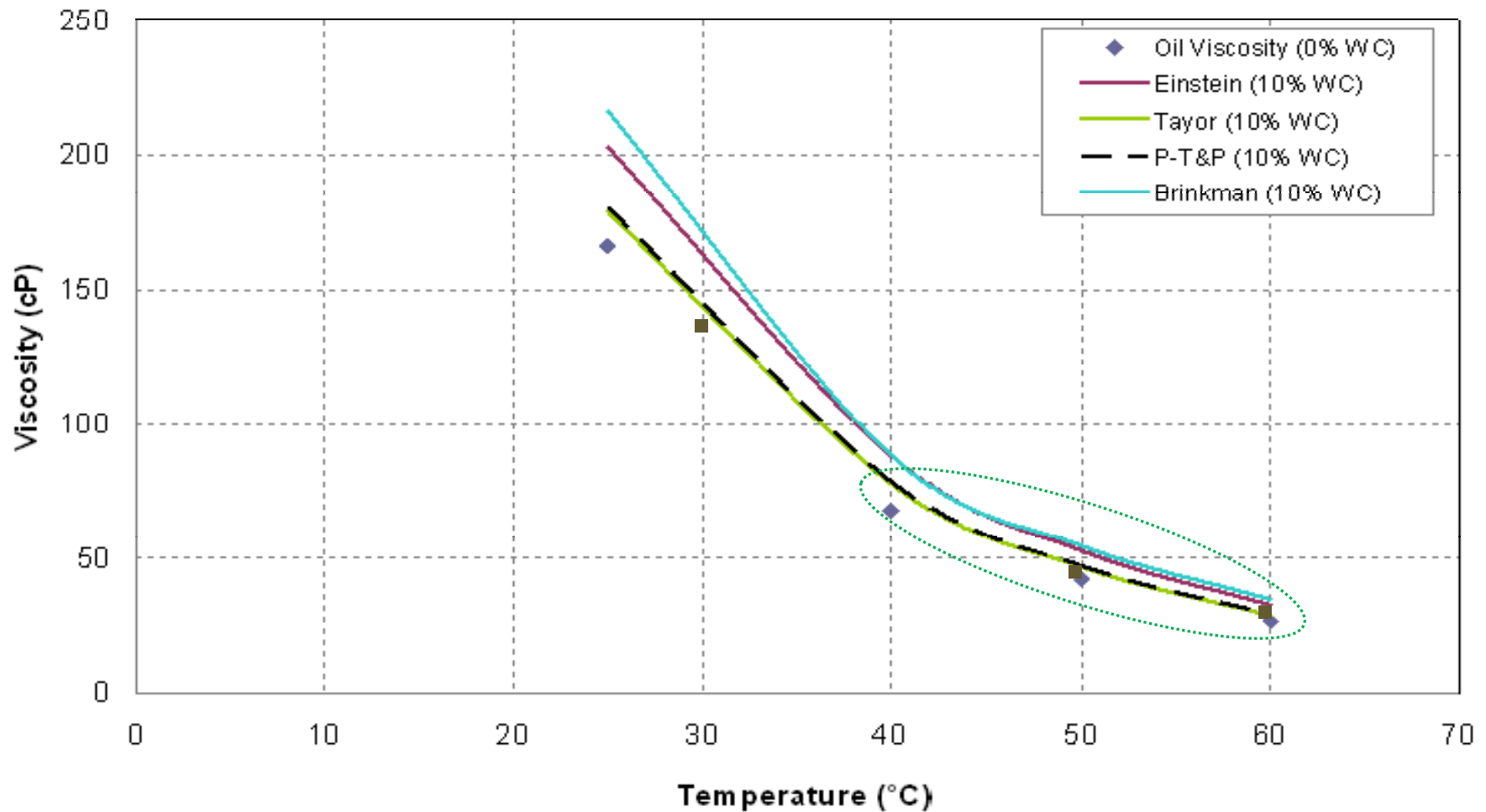
- Transported crude oils with different rheological properties, 19-21° API, water-cuts 5%-30%.
- Viscosity of water-in-oil emulsions tend to increase with the water-cut.
- Field measured fluid properties were used to compare and validate the emulsion viscosity models.
- After a detailed comparison, it was found that the Phan-Thien & Pham (P-T&P) correlation and Taylor correlation yield very similar results.



Viscosity Model Selection



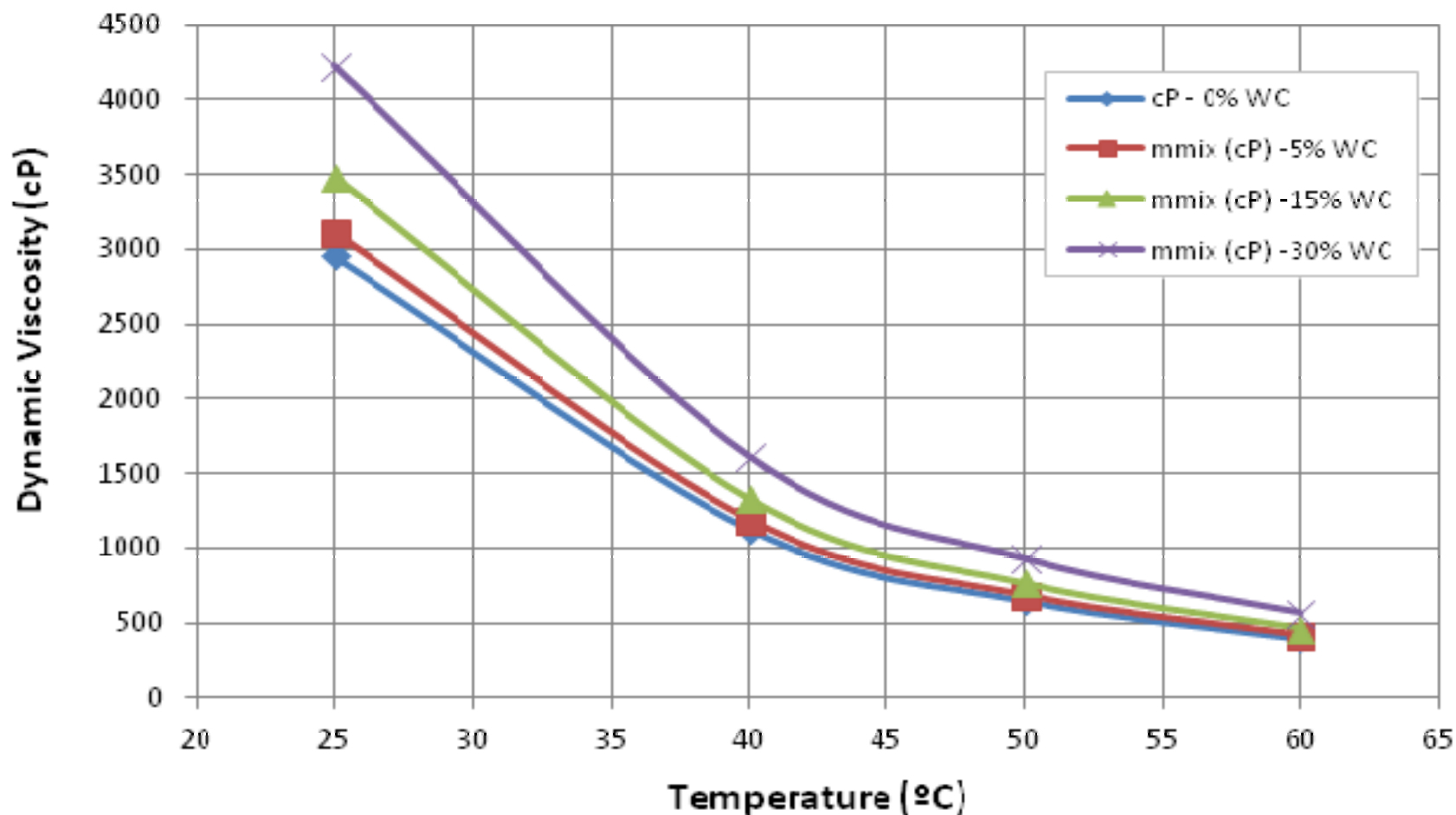
**Dynamic Viscosity versus Temperature Correlation Comparison
for a 10% Water-Cut (WIO)**



Phan-Thien & Pham Model



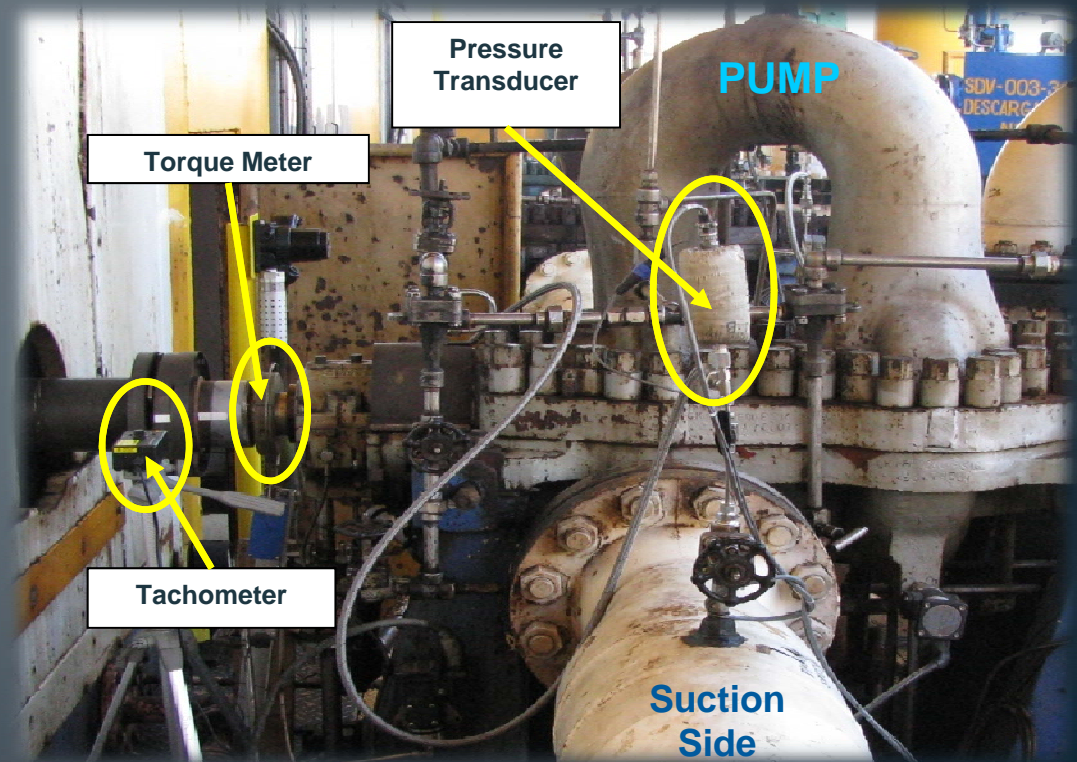
Dynamic Viscosity for Different Water-Cuts for a 16° API Crude Oil versus Temperature



Field Activities & Testing



- Two visits to the Rebombeo platform of PEMEX.
- Operational data and performance testing of various pumping equipment.
- The tests were performed following the guidelines provided in the ASME PTC 8.2.
- Transient and steady-state data including start-up, shutdown, and steady-state for each pump.

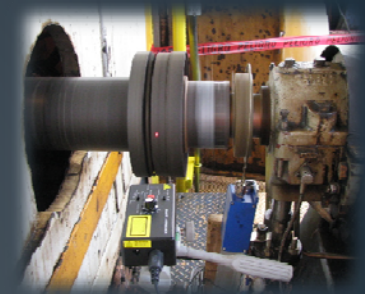


Field Measurements



- **Measured Parameters:**

- Pump speed (digital tachometer)
- Flow rate (doppler, ultrasonic, and orifice plate)
- Shaft torque (telemetric system)
- Suction, discharge, and differential pressure (PTs and DPT)
- Inlet and outlet pump temperature (RTDs)
- Accelerometers



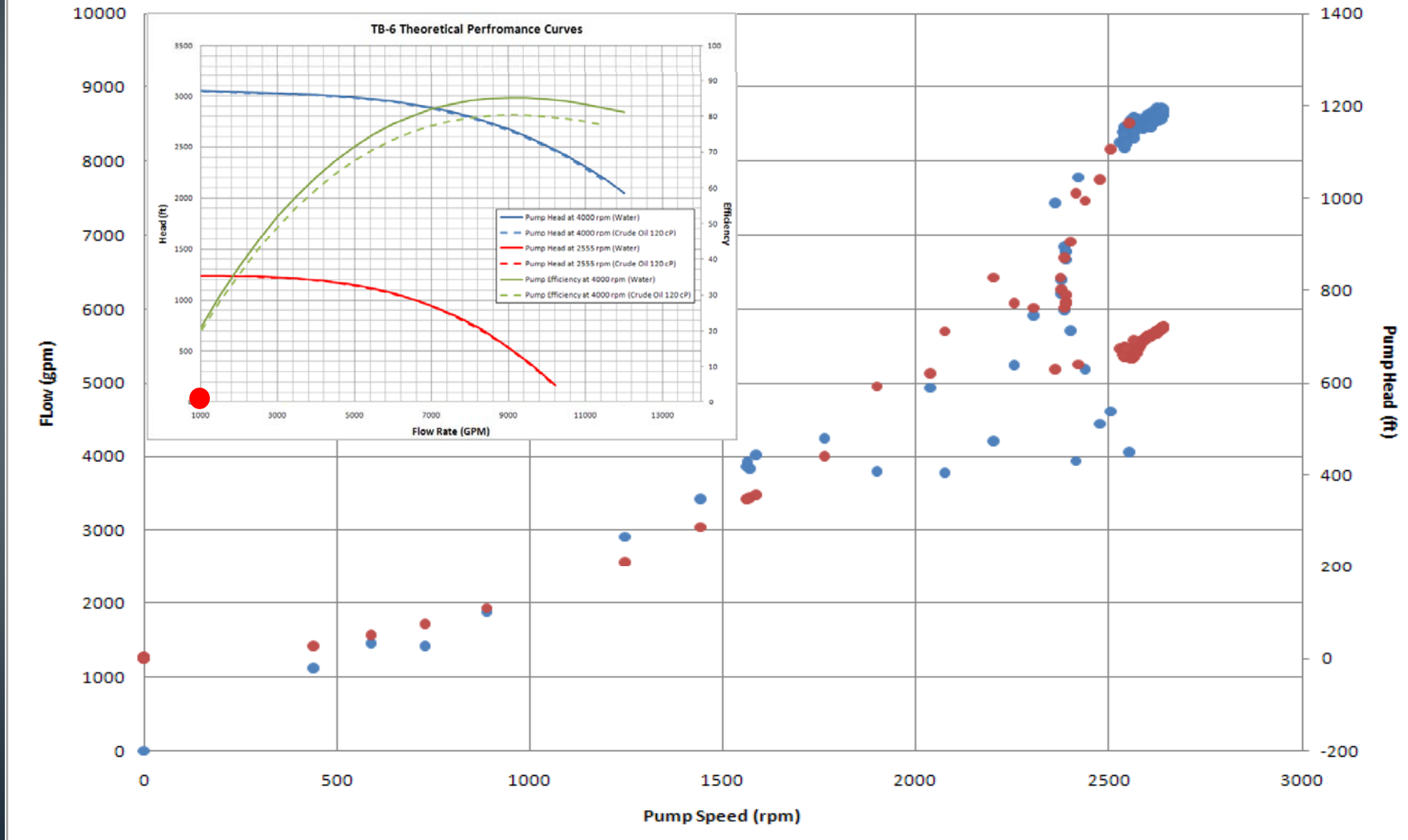
- **Test characteristics:**

- At least 8 points between the 25% of the specified capacity or minimum and maximum flow of the pump for test capacity
- The tests were performed based on the Performance Testing Code ASME PTC 8.2, considering the limitation of the system and operation constraints (flow control logistic)

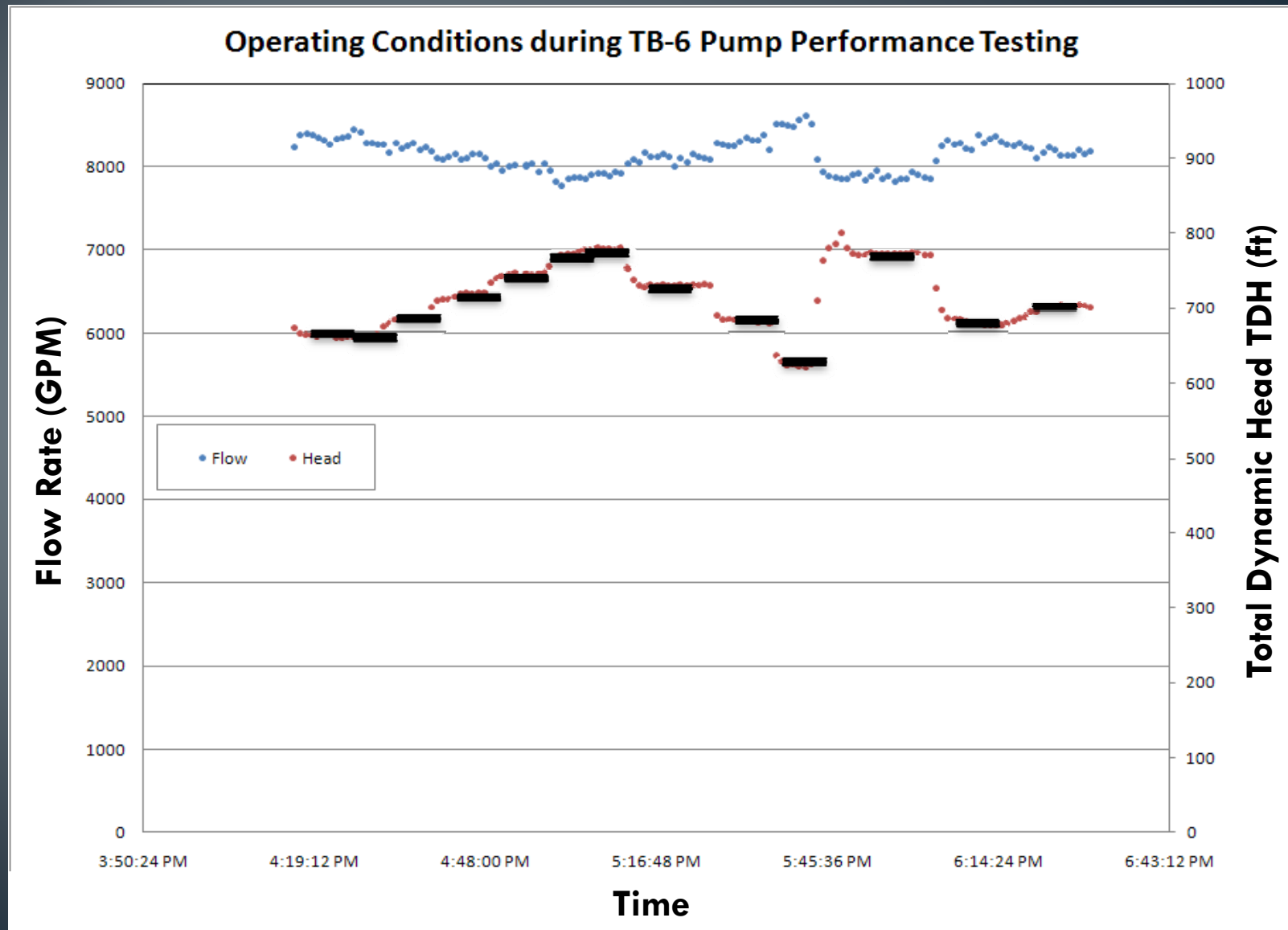
Transient Data – Pump Start-Up



TB-6 OPERating Conditions during Start-up on 08/18/2010



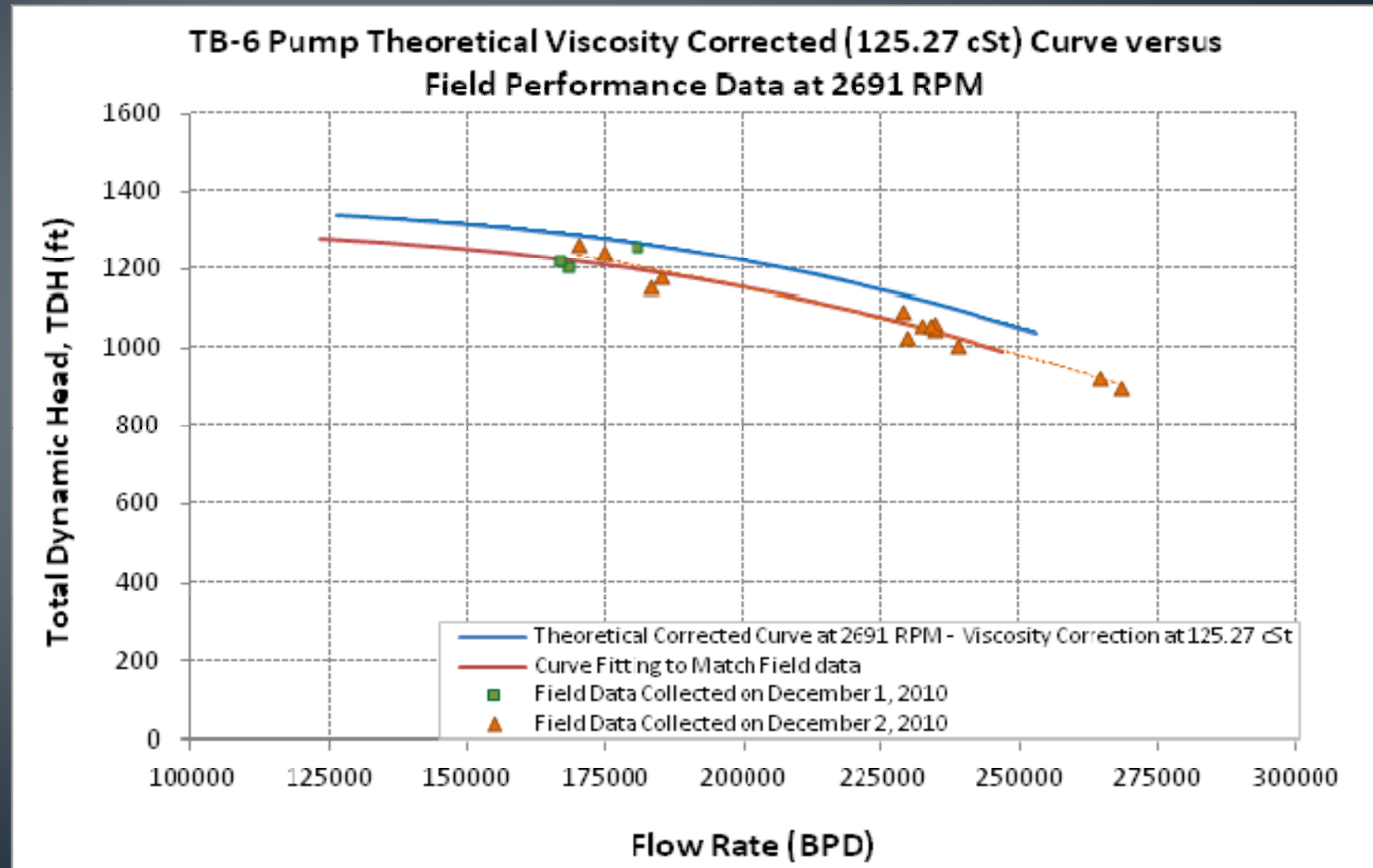
Performance Testing of TB-6



Performance Test Results – TB6



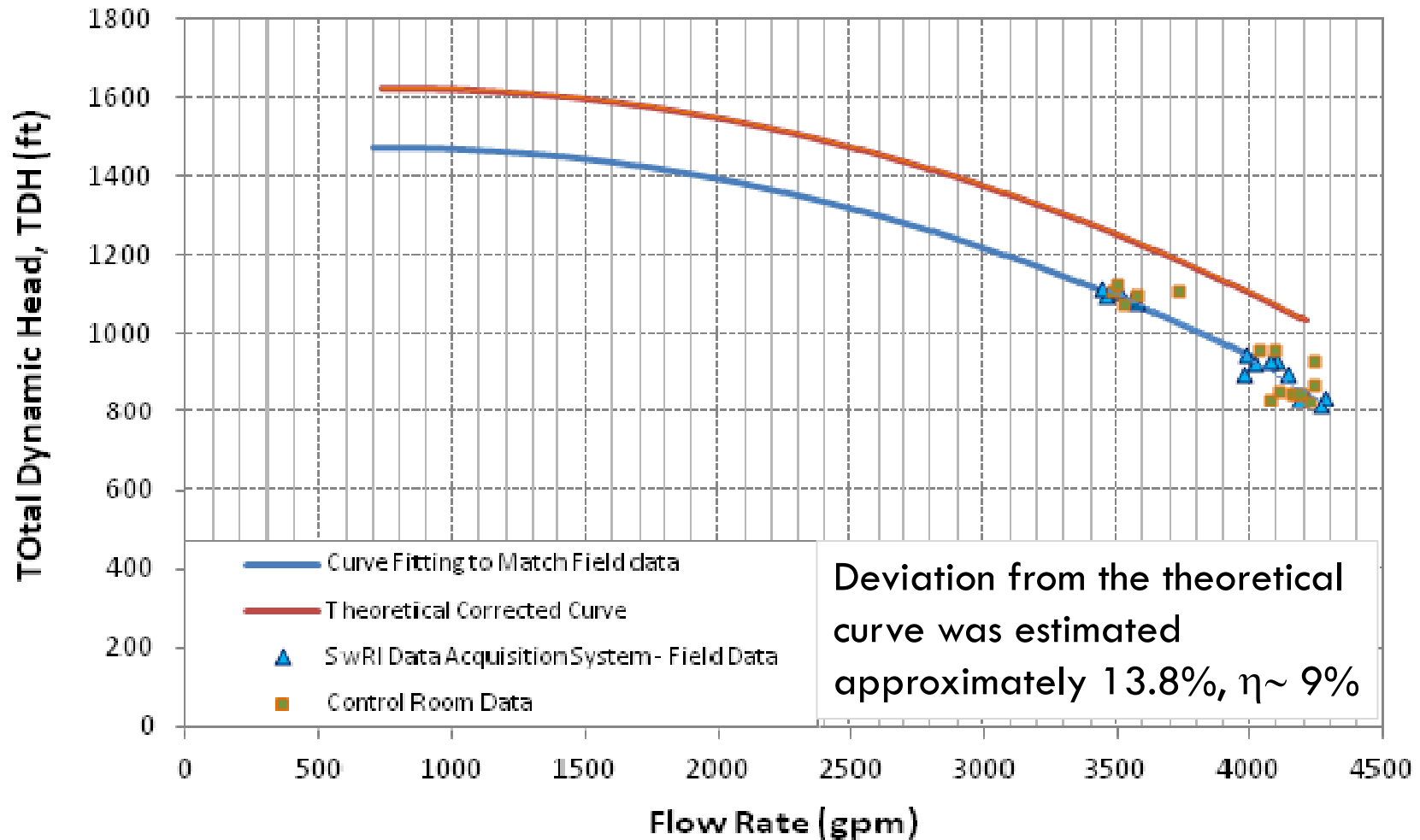
Average deviation from the head curve was estimated about 4.47%



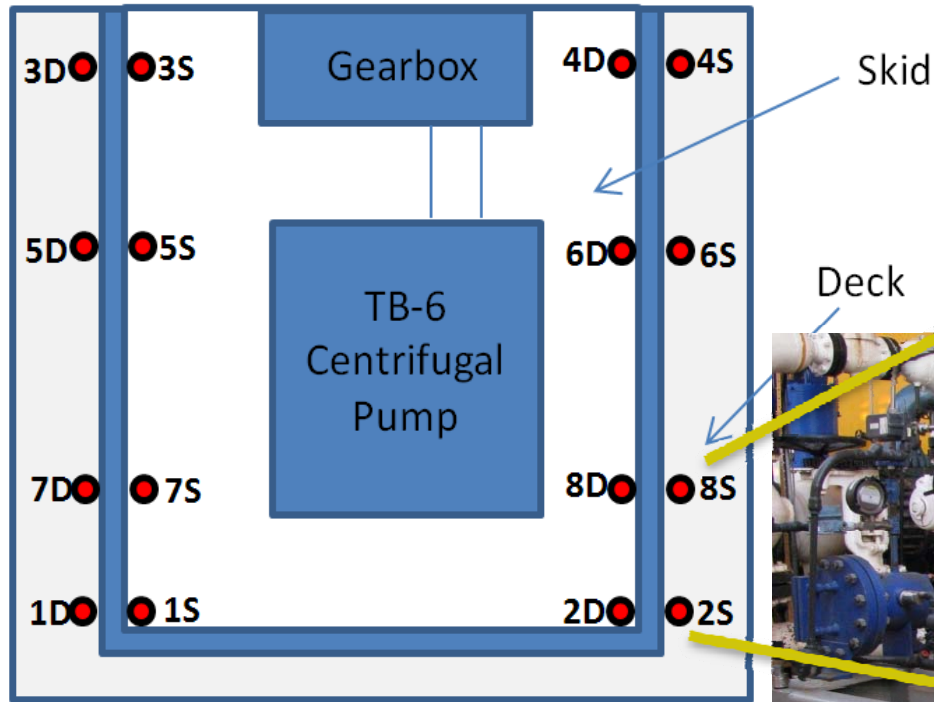
Performance Test Results – TB4



Theoretical Viscosity Corrected (125.27 cSt) Curve versus Field Performance at 4827 RPM fro TB-4 Pump



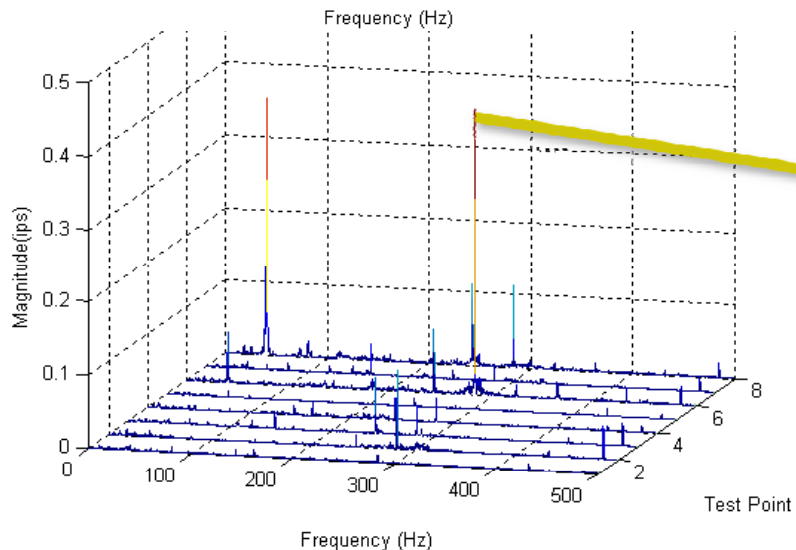
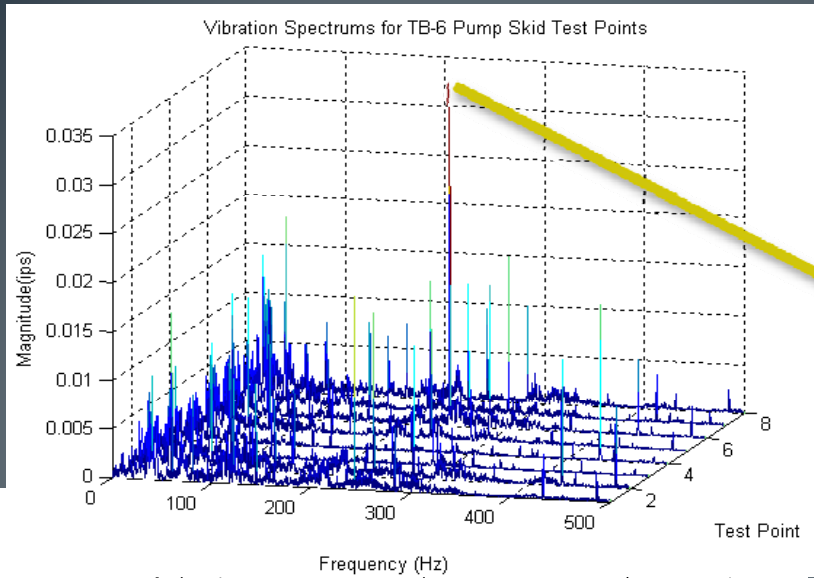
Vibration Measurements



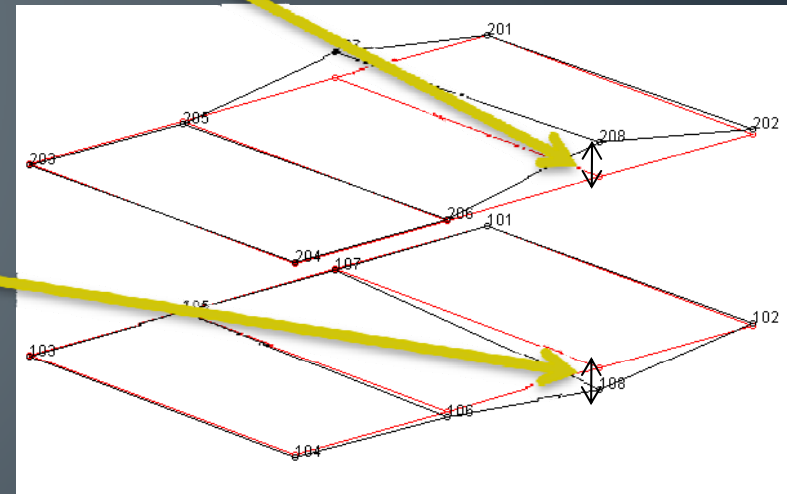
Vibration on the TB-6



This values only apply to the frame side (201-208)



Classification of Vibration	Velocity (0-pk), Inches/sec	Velocity (0-pk), mm/sec
Smooth	< 0.2	< 5.1
Acceptable	0.2 – 0.3	5.1 – 7.6
Marginal	0.3 – 0.4	7.6 – 10.2
Planned Shutdown Repairs	0.4 – 0.6	10.2 – 15.2
Immediate Shutdown	> 0.6	> 15.2



The maximum obtained vibration values were within 0.1-0.3 ips (inch per seconds) at 1X which are considered low and acceptable

Modeling Analysis

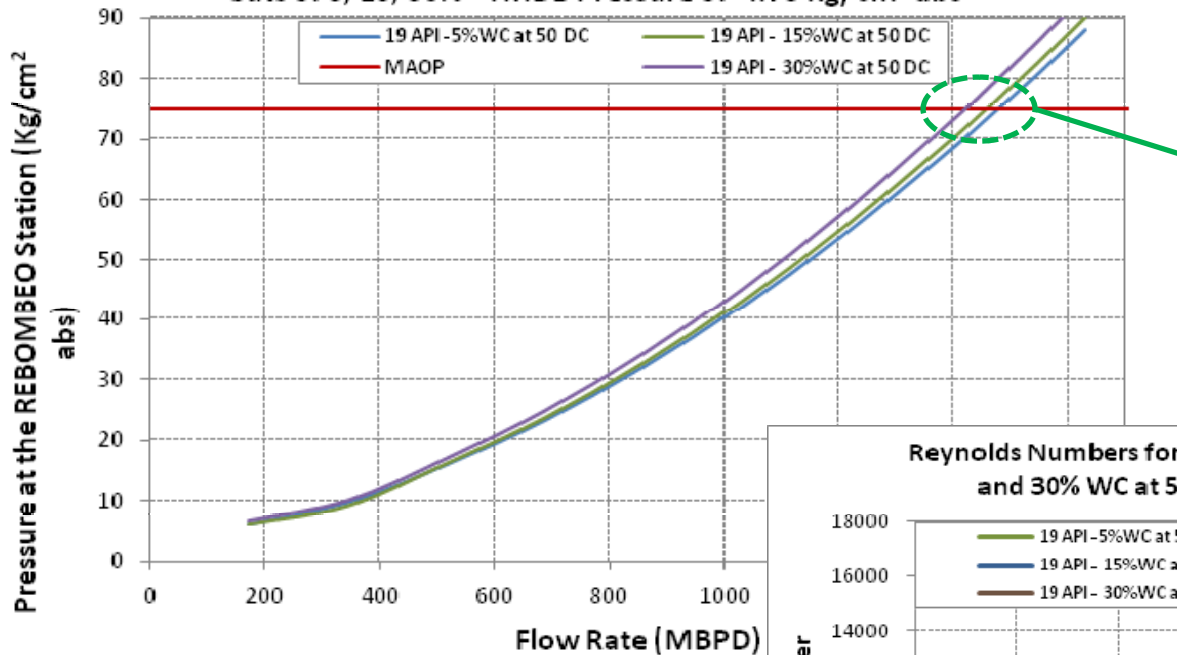


- **The conditions evaluated include:**
 - Two different crude oils, 16° API and 19° API
 - Two temperatures, 50°C and 61°C
 - Three water-cuts, 5%, 15%, and 30%
 - Two pipeline configurations, L2 and L1+L3
 - Two suction pressures, normal (7.5 kg/cm²) and minimum (4.5 kg/cm²)
- **Equipment configuration:**
 - 6 centrifugal pumps (4 low capacity + 2 high capacity)
 - 4 low capacity centrifugal pumps
 - 4 double screw pumps (future configuration)

System Curves



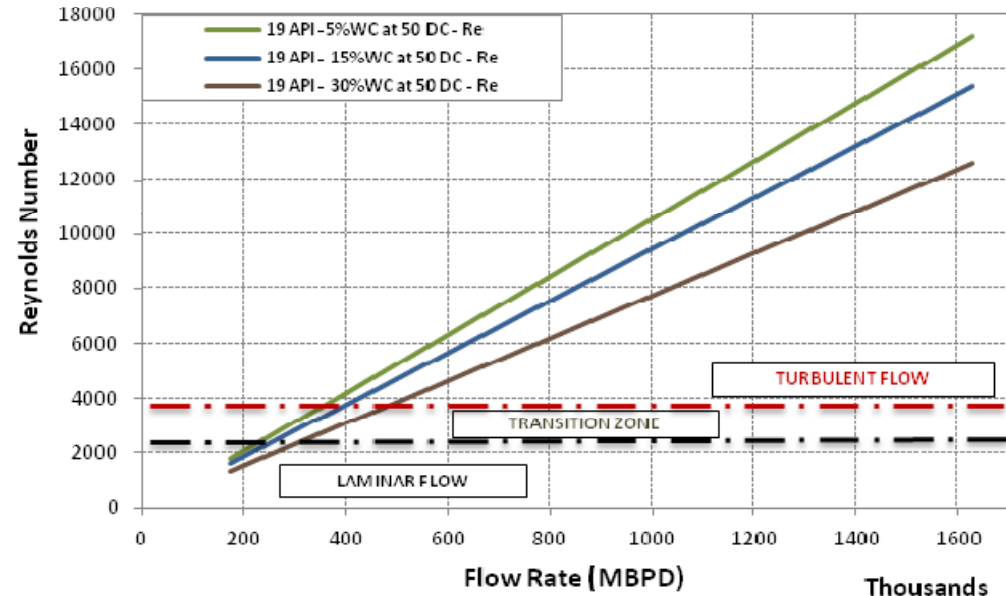
System Curves for L1 + L3 with a 19° API Crude at 50 DC and Water-Cuts of 5, 15, 30% - TMDB Pressure of 4.73 Kg/cm² abs



Calculated capacity of approximately 1.42-1.47 MMBOPD for the presented conditions

Regimen transition at very low flow rates

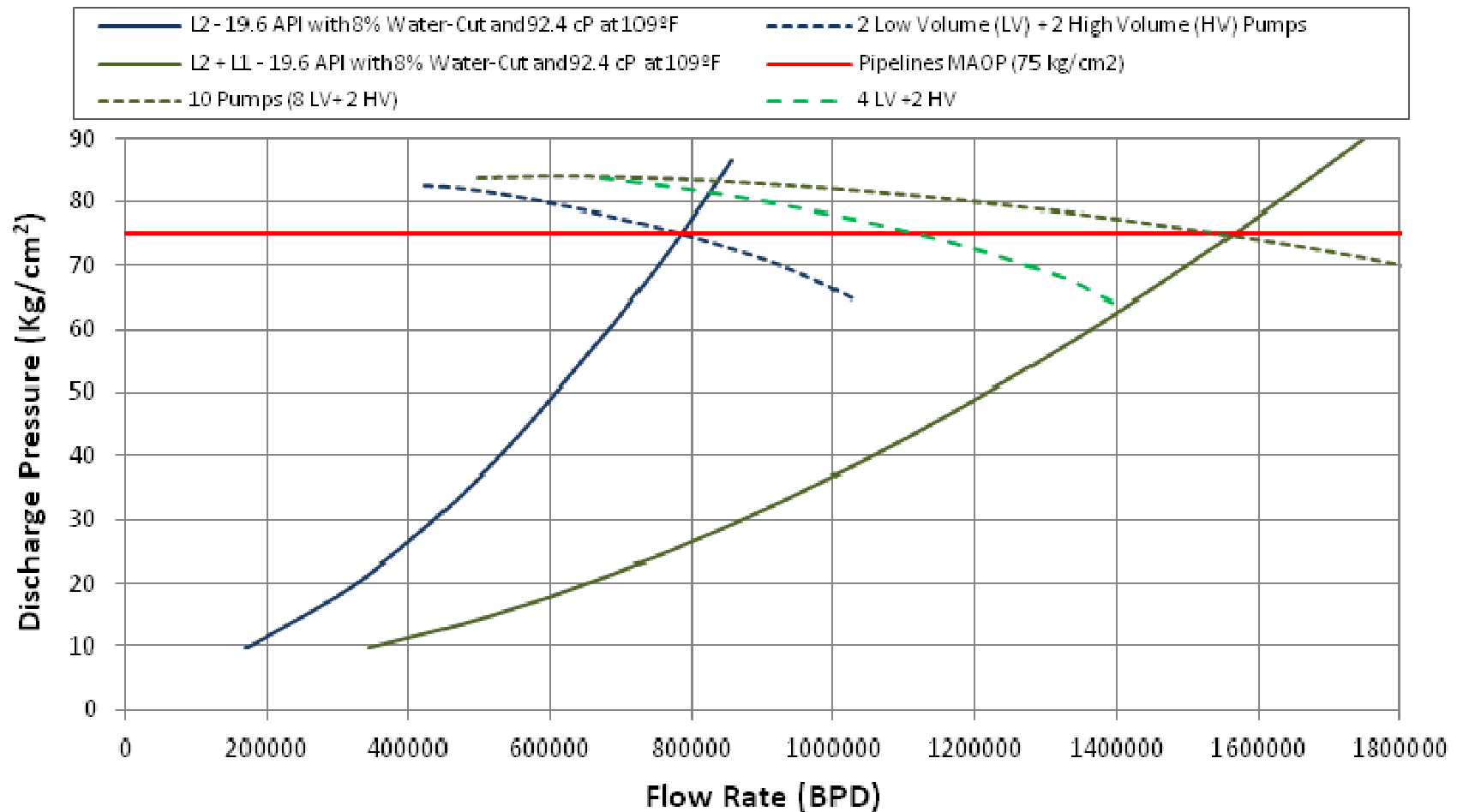
Reynolds Numbers for L1 + L3 System with a 19° API Crude with 5, 15 and 30% WC at 50 DC - TMDB Pressure of 4.73 Kg/cm² abs



System and Pump Curves



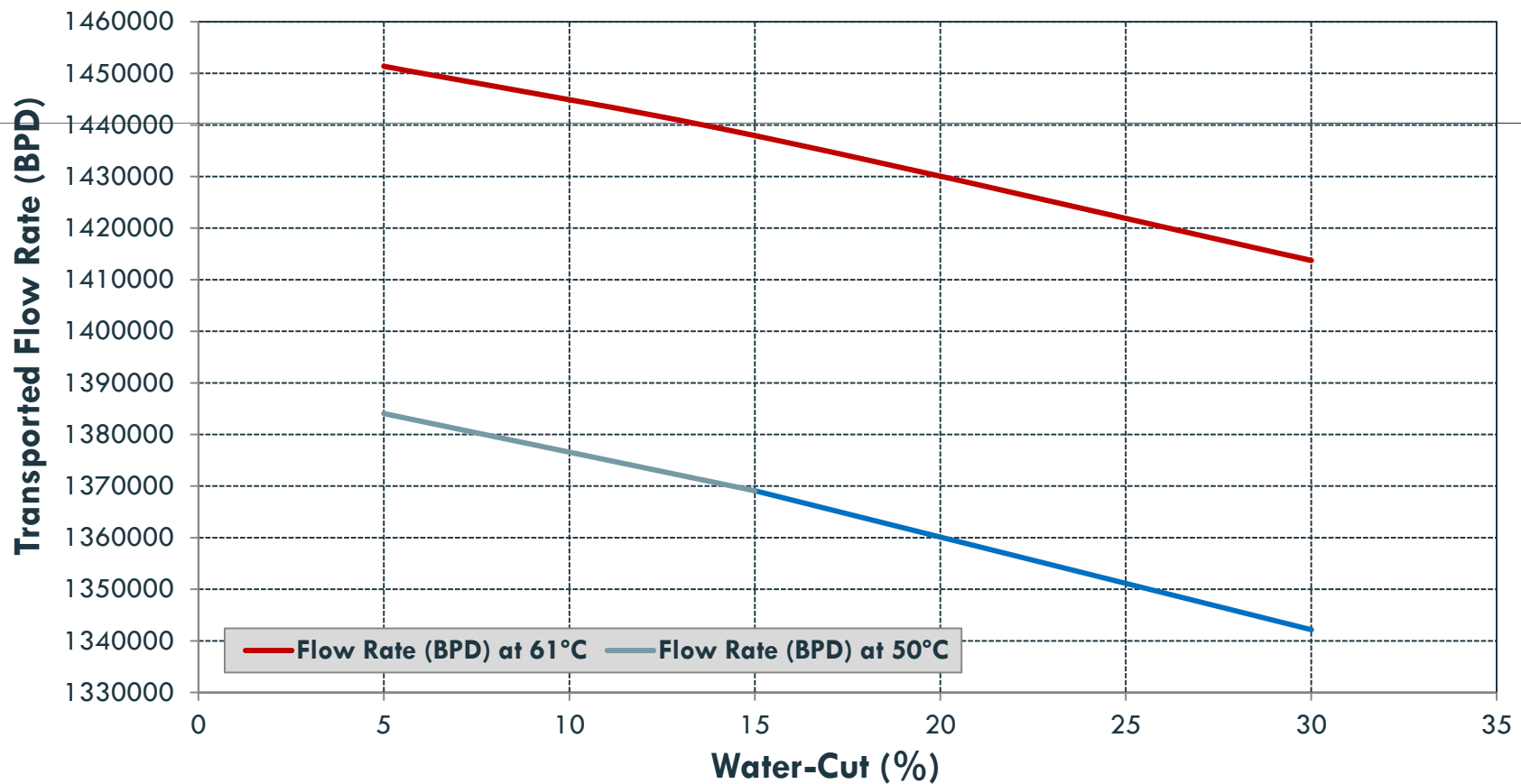
System and Pump Curves for the L2 and L1 Operating with a 19.6 API Crude Oil with a Dynamic Viscosity of 92.4 cP at 109° F and 8% Water-Cut, Constant Suction Pressure of 7.5 Kg/cm² and TMDB Back Pressure of 3.7 Kg/cm²



Effect of the Water-Cut on the Capacity



**Flow Rate through L1 and L3 with the LV and HV Pumps
Transporting a 19°API Crude Oil at Different Water-Cuts and
Two Temperatures**

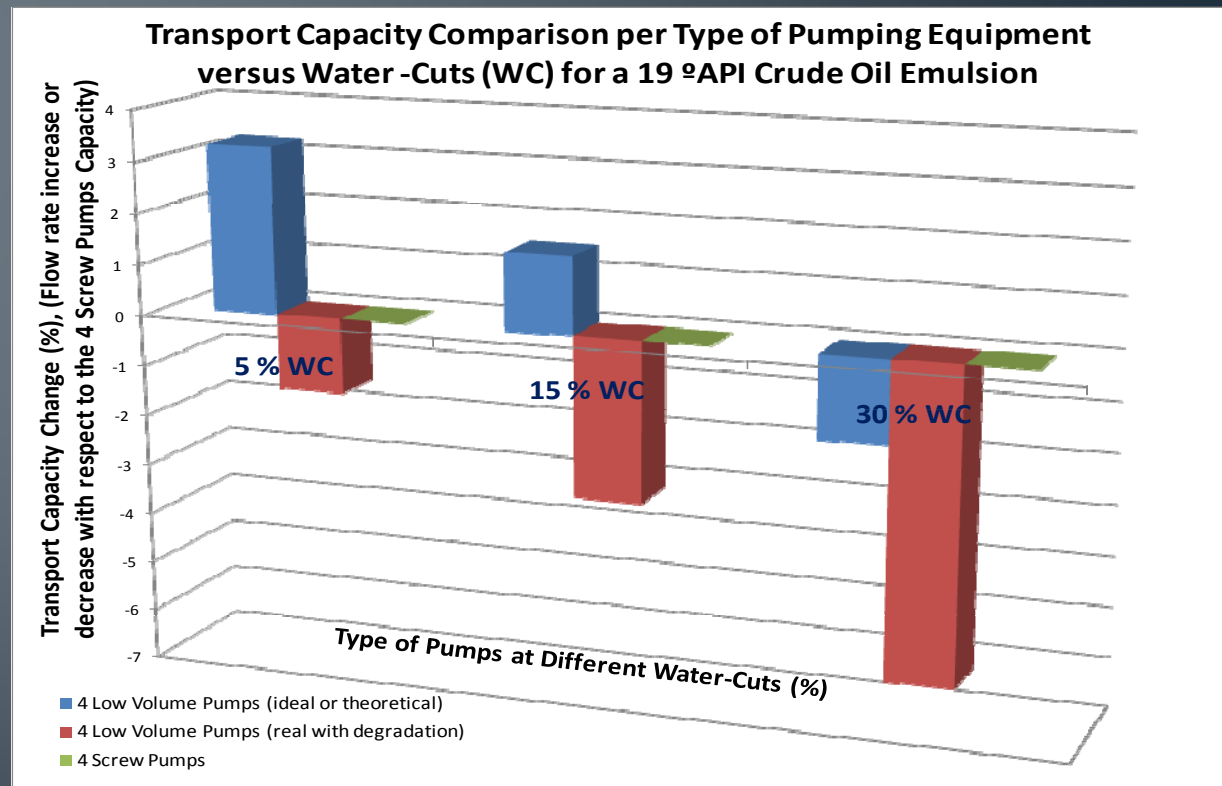


Double Screw Pumps Modeling Results



- 4 new double screw pump trains with 19.6° API
- Higher flow rate of about 1.48% to 6.19% with the screw pumps for water cuts of 5% and 30%, respectively
- 4 new double screw pump trains with 16° API

It was estimated an increase in pumping capacity of approximately 13.28% with the double screw pumps when the system is operated with 16° API and 4 LV pumps only.



Summary and Conclusions



- Volumetric pumps degradation was measured in the field and incorporated in the hydraulic model.
- High viscosity fluid affect significantly the performance, efficiency, and power consumption of the centrifugal pumps. The ANSI/HI 9.6.7-2004 provides a good methodology for correcting the performance curves within a 3-5% difference against measured data.
- Simulation cases allowed calculating the system curves and the current maximum capacity and the forecasted future flow condition with a heavier crude oil.
- System capacity calculated with the existing centrifugal pumps was compared against new screw pumps yielding a 6.19% and 13.24% increase in capacity for the 19° API and 16° API, respectively.
- The results obtained in this study provided good basics for supporting the selection of the new screw pump equipment.

Acknowledgements



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THANKS!



Platform Location →

