



# **INTRODUCTION TO SAMPLING FOR MINERAL PROCESSING**

**Part 7 in a series  
“Effects on Recovery  
and NSR”**



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# Detrimental effects to operations

The assays from samples are used for control and accounting purposes:

- Planning
  - Production targets
  - Plant need to make a certain amount of money to pay its bills and make a profit. This effects how much tonnage to push through a mill.
- **Plant control**
  - **Grade / Recoveries**
  - **Target values for these are set and accurate, non-biased, assays are required to achieve this.**
- Metallurgical Accounting
  - Unbalanced results (poor sampling, assaying or weighing of stream)
  - Unaccounted loss (lack of measurement accuracy)

# How is sampling inaccurate

## Problem with samplers which do not adhere to sampling theory:

- Launder and pressure samplers contain a bias, or errors, which can be constant (biased) or fluctuating (random). The ratio of fines:coarse, or light:heavy, particles entering the fixed cutter or nozzle will vary even without fluctuations in the process.
- Segregation by particle size, density, etc. is always present as there can be no guarantee that the slurry to be sampled is homogenous
- Segregation caused by pipe bends or intersections, etc.
- Unfortunately these errors change over time due to fluctuations in feed tonnages, particle size, densities, flow rates, pressure, etc. which can cause precision errors



# OSA and Sampler Errors (On-line Assays)

- On-Stream Analyzers (OSA) only analyze the samples it is presented
- Normal OSA accuracies, as 1-SD (depends on application)
  - Feed ~ 4-6% (Aver 5%), Conc ~ 2-4% (Aver 3%), Tails ~ 7-9% (Aver 8%)
- Measurement result error (1-SD):
  - :  $S^2_{meas} = S^2_{sampling} + S^2_{analytical}$
  - :  $S_{meas} = \sqrt{S^2_{sampling} + S^2_{analytical}}$
- If the sample feed to the OSA is biased, the results are biased



A is Feed  
B is Conc  
C is Tail

# Error Propagation - Recovery

Error Propagator

	Value	Error
A	1.75	0.09135
B	13.5	0.45280
C	.25	0.02035
D		
E		
F		
G		
H		
I		
J		
K		
L		
M		
N		
O		
P		
Q		
R		
S		
T		
U		
V		
W		
X		
Y		
Z		

Equation:  
 $100*B/A*(A-C)/(B-C)$

Operators:  
Log() In() e^() 10^() Sqrt() EE()  
exp() Sin() Cos() Tan() Log(V,B) X^(2)  
abs() aSin() aCos() aTan() Pi e

Compute

Computed Value:  
**87.33153638814017**

Computed Error:  
**1.297780317295496**

Error Propagator

	Value	Error
A	1.75	0.08923
B	13.5	0.42691
C	.25	0.02016
D		
E		
F		
G		
H		
I		
J		
K		
L		
M		
N		
O		
P		
Q		
R		
S		
T		
U		
V		
W		
X		
Y		
Z		

Equation:  
 $100*B/A*(A-C)/(B-C)$

Operators:  
Log() In() e^() 10^() Sqrt() EE()  
exp() Sin() Cos() Tan() Log(V,B) X^(2)  
abs() aSin() aCos() aTan() Pi e

Compute

Computed Value:  
**87.33153638814017**

Computed Error:  
**1.279411606606388**

## CASE1

Feed% 1.75  
Conc% 13.50  
Tail% 0.25  
Rec% 87.33

Errors % (1-SD) Case1 OSA ABSTotal  
Feed 1.50 5 0.09135  
Conc 1.50 3 0.45280  
Tails 1.50 8 0.02035

Recovery error 1.2978

## CASE2

Feed% 1.75  
Conc% 13.50  
Tail% 0.25  
Rec% 87.33

Errors % (1-SD) Case2 OSA ABSTotal  
Feed 1.00 5 0.08923  
Conc 1.00 3 0.42691  
Tails 1.00 8 0.02016

Recovery error 1.2794

Recovery Error Difference  
0.0184 (1-SD)

# Grade / Recovery

- This statement can be found in the Will's Mineral Processing Technology book:

**“The aim (of a flotation control system) should be to improve the metallurgical efficiency, i.e. to produce the best possible grade-recovery curve, and to *stabilize the process at the concentrate grade* which will produce the most economic return from the throughput.”**

- This statement has a few key points:
  - A concentrate grade is decided upon ( could be by planer, metallurgist, control system or other and depends on feed grade)
  - Keep the process stable ( upsets are not good)
  - Increase the recovery as close as possible, to the best grade-recovery curve, without de-stabilizing (upsetting) the circuit
  - Maximize recovery at a target grade



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# Assay errors and Grade/Recovery curve

Feed %1.75, Conc. %13.5 Tail %0.25, Rec. %87.33

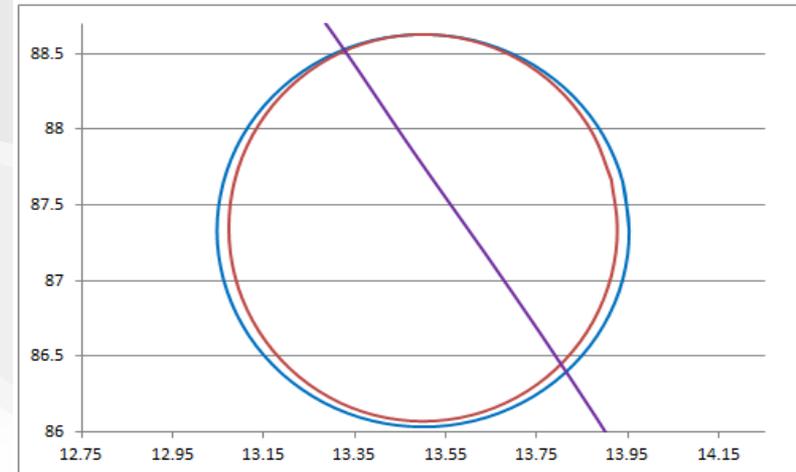
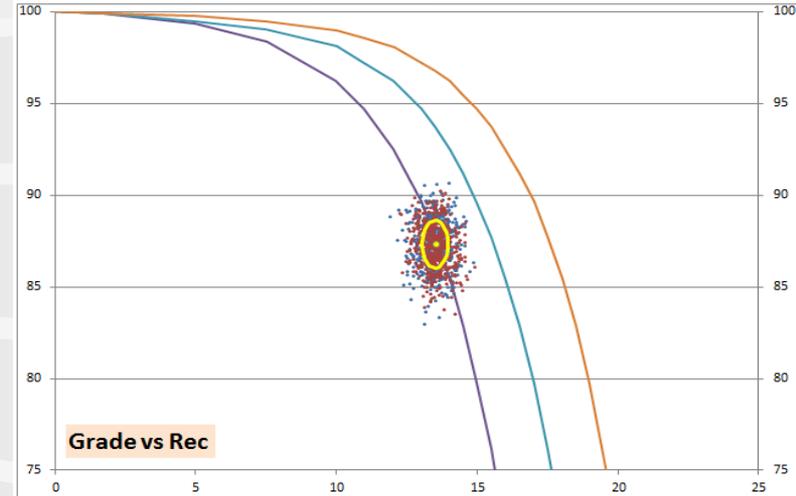
	Case 1(1.5%)	Case 2(1.0%)
Recovery error	1.2978	1.2794
<b>Recovery Error Difference 0.0184 (1-SD)</b>		

## Uncertainty Ellipse Area

%Grade x %Rec	1.85	1.72
<b>Control Area Improvement % 7.06</b>		

## COMMENTS

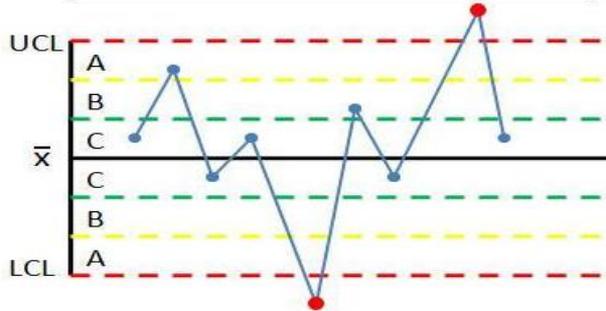
- With the slightly better samplers in Case 2, the recovery target can be moved upwards the 0.0184% ( or 0.0368% with 2-SD) error difference with the same probability of detecting an upset in the circuit as in Case1
- As the target for grade / recovery changes, due to feed changes, the error difference changes only slightly. (~10%).



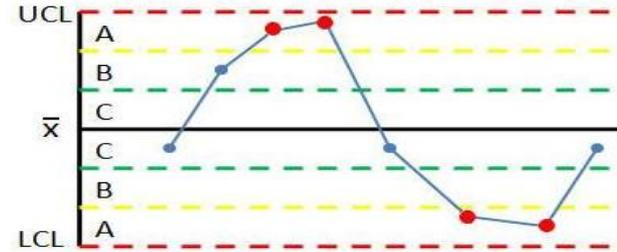
# Introduction to SPC

*“All control starts with measurement and the quality of control can be no better than the quality of the measurement input.” (Connell [1988])*

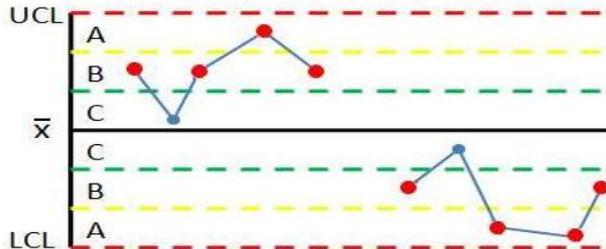
Rule 1: Any point falls beyond  $3\sigma$  from the centerline (this is represented by the upper and lower control limits).



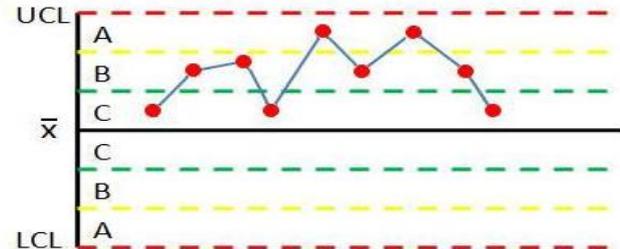
Rule 2: Two out of three consecutive points fall beyond  $2\sigma$  on the same side of the centerline.



Rule 3: Four out of five consecutive points fall beyond  $1\sigma$  on the same side of the centerline.



Rule 4: Nine or more consecutive points fall on the same side of the centerline.



# Introduction to SPC

- Control limits for grade / recovery depend upon the accuracy of the analyzer / samplers
- Example chart of recovery control, target shifted up 1-SD difference, 0.0184%



Probability of error detection over 2-SD UCL is still better than in Case #1

Probability of error detection over 1-SD UCL is the same in both cases

Target moved up 1-SD difference ( 0.0184 )

Tighter control limits at 1-SD LCL and 2-SD LCL



# Error Propagation - \$NSR/t

- Feed %1.75, Conc. %13.5 Tail %0.25
- \$NSR/t \$149.78

	<b>Case 1(1.5%)</b>	<b>Case 2(1.0%)</b>
<b>\$NSR/t error</b>	<b>9.3848</b>	<b>9.1660</b>

**\$NSR/t Error Difference 0.2188 (1-SD)**

Estimate NSR Improvements v2.0

File Help

Assays%		S1 Error		S2 Error		OSA Error		T1 Error	T2 Error
1.75	Feed in %	1.5 %		1 %		5 %		0.0914	0.0892
13.5	Conc in %	1.5 %		1 %		3 %		0.4528	0.4269
0.25	Tail in %	1.5 %		1 %		8 %		0.0203	0.0202

NSR Par's

14330	Metal Price \$/t
87	Smelter Payment %
350	Treatment \$/t
10	Transport \$/t
2.102400	Tons Processed Mt

Update Calculations

**RESULTS**

		S1 SD	S2 SD	SD Diff
87.33	Recovery %	1.2977	1.2792	0.0185
149.78	NSR \$/t	9.3848	9.1660	0.2188
314.9	MS/(mo,yr)			

**IMPROVEMENTS**

7.06	%grade/%rec
7.92	%grade/\$NSR
0.460	MS/(mo,yr)



# Estimating Assay Error Effects on NSR

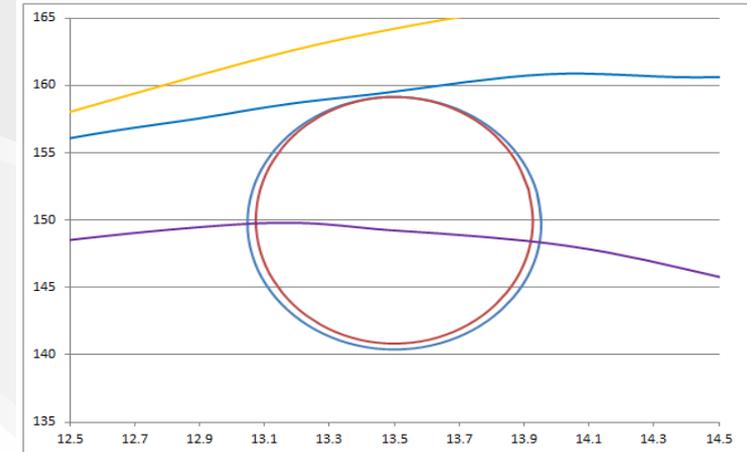
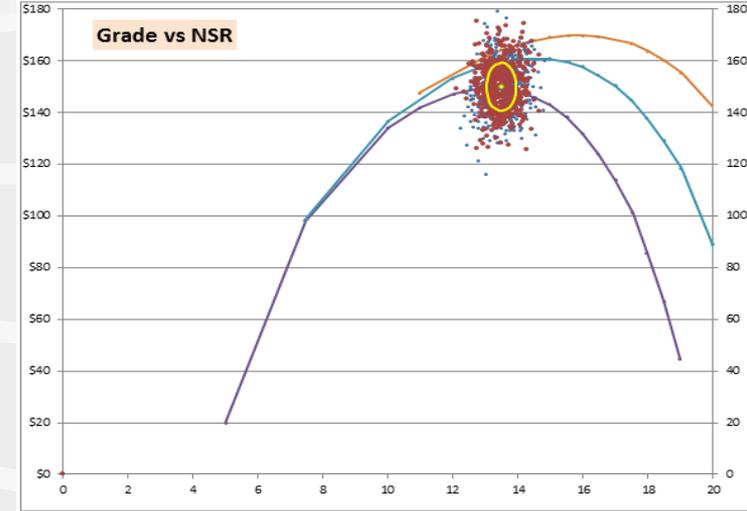
Feed %1.75, Conc. %13.5 Tail %0.25, Rec. %87.33

	Case 1(1.5%)	Case 2(1.0%)
\$NSR/t error	9.3848	9.1660
\$NSR/t Difference	0.2188 (1-SD)	

Uncertainty Ellipse Area	Case 1(1.5%)	Case 2(1.0%)
%Grade x \$NSR/t	13.35	12.29
Control Area Improvement %	7.92	

## COMMENTS

- With the slightly better samplers in Case 2, the \$NSR/t can be moved upwards the \$0.2188 ( or \$0.4376 with 2-SD) error difference with the same likelihood of detecting an upset circuit as in Case1. This is done by the recovery control.
- At 2,102,400 t/year this is:
  - \$459,786.00 @ 1-SD Error Diff
  - \$919,572.00 @ 2-SD Error Diff

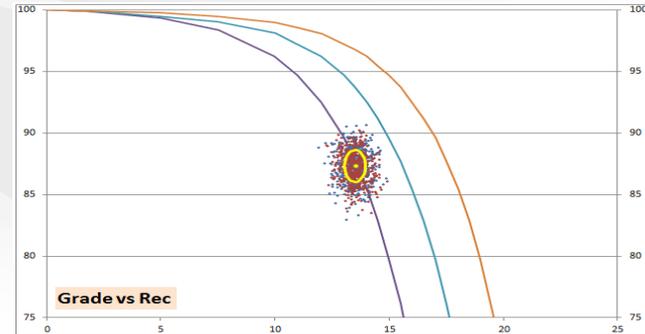
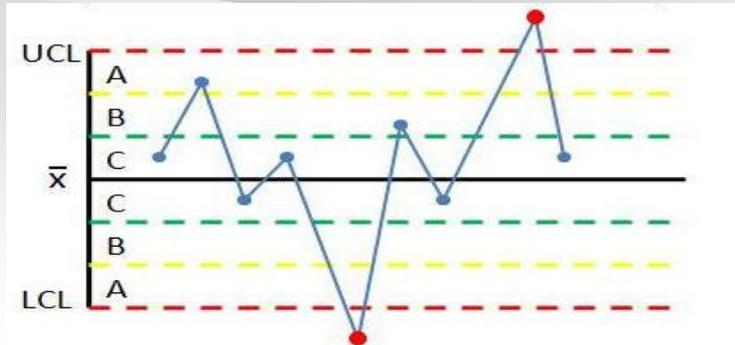




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# Estimating where your process operates

- The probability of process upset as a result of analysis errors at the UCL's are, 1-SD is 16%, 2-SD is 2.25%, 3-SD is 0.15%. An upset occurs where your process crosses the grade / recovery curve.
- Your OSA has about 100 cycles a day , roughly a 15 minute cycle time ( 4/hr x 24hr ~ 100 )
- How often a day does you process get upset?
  - At 8/shift (16/day) your SD is about 1 (x)
  - At 2-3/shift (5-6/day) your SD is somewhere around 1.5 (x)
  - At 1-2/shift (2-4/day) your SD is somewhere around 2 (x)
  - Once every several days, your SD is somewhere around 3
- This gives you an idea of how much you can increase your recovery / NSR target (  $x * 1\text{-SDdiff}$  )





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# Another example (1/2)

- Low grade Cu mine with large tonnages (140,000t/day)
- Comparing 2% and 1% sampler errors
- **\$0.045/t** estimated improvement
- **\$2.19M/yr** estimated improvement
- Control improvements 15.06% and 16.93%

Estimate NSR Improvements v2.0

File Help

Assays%		S1 Error		S2 Error		OSA Error		T1 Error	T2 Error
0.28	Feed in %	2	%	1	%	5	%	0.0151	0.0143
41	Conc in %	2	%	1	%	3	%	1.4783	1.2965
0.022	Tail in %	2	%	1	%	8	%	0.0018	0.0018

NSR Par's

6614	Metal Price \$/t
92	Smelter Payment %
125	Treatment \$/t
70	Transport \$/t
48.545	Tons Processed Mt

**RESULTS**

		S1 SD	S2 SD	SD Diff
92.19	Recovery %	0.7708	0.7466	0.0243
14.48	NSR \$/t	0.8534	0.8083	0.0451
702.9	MS/(mo,yr)			

**IMPROVEMENTS**

15.06	%grade/%rec			
16.93	%grade/\$NSR			
2.191	MS/(mo,yr)			



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# Another example (2/2)

- Low grade Cu mine with large tonnages (140,000t/day)
- Comparing **3% and 1%** sampler errors
- **\$0.115/t** estimated improvement
- **\$5.60M/yr** estimated improvement
- Control improvements 31.28% and 34.78%

Estimate NSR Improvements v2.0

File Help

Assays%		S1 Error		S2 Error		OSA Error		T1 Error	T2 Error
0.28	Feed in %	3	%	1	%	5	%	0.0163	0.0143
41	Conc in %	3	%	1	%	3	%	1.7395	1.2965
0.022	Tail in %	3	%	1	%	8	%	0.0019	0.0018
NSR Par's									
6614	Metal Price \$/t								
92	Smelter Payment %								
125	Treatment \$/t								
70	Transport \$/t								
48.545	Tons Processed Mt								
<input type="button" value="Update Calculations"/>									
<b>RESULTS</b>		S1 SD	S2 SD	SD Diff					
92.19	Recovery %	0.8097	0.7466	0.0631					
14.48	NSR \$/t	0.9237	0.8083	0.1154					
702.9	MS/(mo,yr)								
<b>IMPROVEMENTS</b>									
31.28	%grade/%rec								
34.78	%grade/\$NSR								
5.604	MS/(mo,yr)								



**For more information you can always contact us at:  
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